



Purifying water with plant-based sustainable solutions: Tannin coagulants and sorbents

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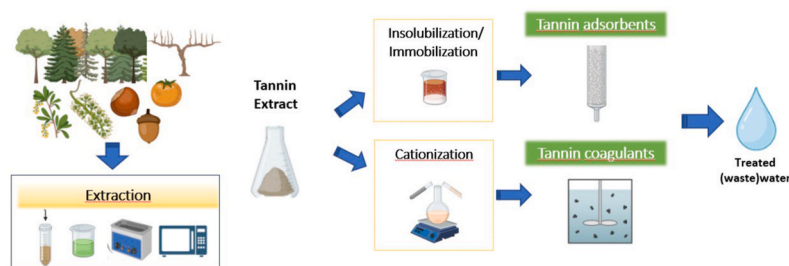
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HIGHLIGHTS

- Tannin as a feedstock for coagulants and sorbents for water treatment.
- Overview of raw materials, synthesis, usage, and pollutant removal mechanism.
- Comparison of tannin coagulants and conventional/commercial coagulants.
- Discussion on potential applications of tannin sorbents.
- More work is needed to obtain valid assessments about cost-efficiency.

GRAPHICAL ABSTRACT



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ABSTRACT

More and more efforts are being made to find efficient bio-based water and wastewater treatment products. Especially the use of tannin-based materials has become more prevalent in recent years due to the wide availability of sustainable tannin sources. This article provides an updated literature review on the potential for tannin use for coagulants and adsorbent synthesis and practical applicability in water purification. Tannin coagulants work well in many applications, especially in color, turbidity, and COD removal from industrial waters, and are often even better than conventional ones (e.g., metal salts). One of the most significant benefits of tannin coagulants is their small effect on the pH of the treated water. Also, tannin coagulants can work at a wide pH range, and sludge volume is typically smaller than with metal salts. However, it is worth noting that the performance varies widely among tannin coagulants. Tannin-derived resins and composites have been synthesized and evaluated as adsorbents for water purification. In general, tannin-derived adsorbents present good adsorption capacities for metals, antimony, cationic dyes, and uranium ions, owing to their chelating ability and negative surface charge in the pH conditions of interest and reducing power in the case of chromium(VI). With simple chemical modifications, tannin can be converted into effective sorbents for more challenging pollutants. More research is needed to test tannin materials on a larger scale and evaluate their overall benefits and cost-effectiveness.

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1. Introduction

Coagulation-flocculation and adsorption are well-established operations in water and wastewater treatment plants. Coagulation-flocculation is an important process for removing colloidal and suspended particles from water. Adsorption is a simple and cost-effective method used at a tertiary treatment level to remove persistent pollutants, including organic micropollutants, metals, and toxic metalloids. Conventional coagulants/flocculants mostly used for water treatment include iron and aluminum-based salts, and synthetic organic polymers. Commercial adsorbents used in large-scale processes include activated carbon, activated alumina, and polymeric adsorbents. Among other possible disadvantages, most of these water treatment materials (e.g., chemical coagulants, coal activated carbons) are produced using non-renewable resources and through energy-intensive processes (e.g., pyrolysis and activation in activated carbon production), generating significant emissions to the environment (Vilen et al., 2022). In the context of stringent regulations, water scarcity, and the need to reduce dependence on primary mining, it is increasingly important to find cost-effective and green technologies to produce potable water and to remediate wastewater. Much work has been done to develop sustainable bio-based coagulants and adsorbents from renewable sources. Especially the use of tannin-based materials has become more prevalent in recent years due to the wide availability of tannin raw materials. Tannins are present in different parts of multiple vegetable species and are easily extracted with water, avoiding organic solvents. They present a high chelating capacity, abundant hydroxyl groups, and many ways of chemical modification (Arbenz and Averous 2015; Vera and Urbano 2021) which explain the increasing recognition of tannin as a raw material for sustainable green industries. The use of tannins as precursors of alternative coagulants/flocculants and adsorbents for water purification is a newly recognized field of application.

Black wattle (*Acacia mearnsii*) and quebracho (*Schinopsis lorentzii*) are the most used source of commercial tannins, also highly investigated as feedstock for coagulants and adsorbents production (Beltrán-Heredia et al., 2012; Sánchez-Martín et al., 2013). Tannin from other plant species such as grape stems, persimmon, spruce, eucalyptus and maritime pine bark, acacia catechu have been researched (Thakur and Choubey 2014; Bacelo et al., 2020; Bello et al. 2020, 2022; Giroletti et al., 2022; Liu et al., 2022; Tomasi et al., 2023) but there is still room for innovation. Evaluating other agro-food and agroforestry residues, as an effort to value locally available materials and reduce the production impact of coagulants/flocculants and adsorbents is essential. Tannins can be extracted by conventional solid-liquid procedures and advanced extraction methods, such as supercritical fluid extraction, pressurized liquid extraction, ultrasound-assisted and microwave-assisted extraction (Ibrahim et al., 2021). The best extraction method and operating conditions should be optimized on a case-specific basis to simultaneously provide good yields and extracts with high-condensed tannin content (Tomasi et al., 2023), minimizing energy and chemical requirements. Purification or isolation of tannin extracts is usually considered unnecessary for coagulants/adsorbents synthesis (Ibrahim et al., 2021), although smaller phenolic compounds, carbohydrates, and inorganics could be extracted along with tannins and affect coagulant ability.

Tannin coagulants provide a sustainable alternative to conventional coagulants. Cationization of tannin extracts can be done by simple Mannich reaction, where formaldehyde and amine react to form an iminium ion, which further reacts with the phenolic rings of the tannin. This results in water-soluble polymer with cationic nature (Graham et al., 2008).

Tannins are water-soluble compounds but can be easily rendered insoluble or immobilized, making them highly valuable as adsorbents. The most common way to insolubilize tannin is through polymerization with an aldehyde (also called gelification), which creates a cross-linked three-dimensional structure (Arbenz and Averous 2015). Auto-condensation of tannin and innovative immobilization procedures

(grafting with chemical moieties and incorporation into composites) have generated adsorbents with enhanced chemical functionality and properties.

Comprehensive reviews have been published on tannin coagulants (Ibrahim et al., 2021; Das et al., 2022; Tomasi et al., 2022), addressing extraction, modification and purification performance, and on adsorbents (Santos et al., 2019; Sadeq et al., 2023). This article presents an up-to-date literature review, offering a comprehensive understanding of the recent advancements on tannins use in water purification, an area that has witnessed rapid progress in last years. Regarding tannin coagulants, the review aims explicitly to summarize findings comparing tannin coagulants with other coagulants. The adsorbents chapter discusses new synthesis routes, critically analyzes the challenges and gaps, and highlights the potential applications.

2. Tannin coagulants for water treatment

2.1. Preparation of tannin coagulants and coagulation mechanism

Most colloidal particles in water are anionic and their destabilization requires cationic coagulant. Cationic tannin coagulants are obtained by introducing amine groups into tannin structure. This can be done by simple Mannich reaction, where formaldehyde and amine react to form an iminium ion, which further reacts with the phenolic ring of the tannin structure and substitutes the hydrogen. Mannich modification of tannin, which have been reviewed recently (Ibrahim et al., 2021; Tomasi et al., 2022), has been done with different amines and by changing reaction conditions such as ratio of amine and formaldehyde, temperature, pH, and reaction time.

The amount of phenolic groups in the tannin structure affect reactivity and thereafter properties of the obtained coagulant. For example, a higher amount of phenolic groups in the quebracho tannin compared to spruce bark tannin resulted in much higher charge density of the quebracho coagulant (Bello et al., 2020). Charge densities of tannin coagulants have typically varied in the range of 0.8–3.8 meq/g (Fang 2007; Bello et al. 2020, 2022; Bello and Leiviskä 2022), which can be referred to as low to medium charge densities. Besides raw material, the tree harvesting season and extraction procedure may have significant effects on the amount of impurities in extracts/coagulants as well as on the charge densities of coagulants. Bello et al. (2022) obtained higher charge densities for spruce tannin coagulants, when they were produced from tannin extracted from winter spruce bark and having a preliminary cold-water extraction prior to the hot-water extraction. This extraction procedure reduced the amount of non-phenolic constituents (impurities) from the winter bark but not from the summer bark.

The main mechanisms for the destabilization of colloidal impurities are the charge neutralization and interparticle bridging mechanisms (Ibrahim et al., 2021). The charge density is pH-dependent due to amine protonation/deprotonation. Graham et al. (2008) showed that the optimal pH for the destabilization of kaolin suspension by a tannin coagulant was at pH 4 due to the charge neutralization mechanism. A higher dosage was needed at higher pH, however lower residual turbidity was obtained due to polymer precipitation and interaction with kaolin particles. Nevertheless, at pH 7, aluminum sulfate (AS) and polydiallyldimethylammonium chloride (polyDADMAC) achieved lower residual turbidity than tannin coagulant (TC).

2.2. Purification efficiency and dosage requirements

Table 1 compares tannin coagulants to other coagulants in water and wastewater treatment in terms of dosage requirements and purification efficiency. They are considered the most important factors in determining the superiority of coagulants, while the floc characteristics, flocculation time, and sludge properties are also critical parameters when considering the overall process. The wastewater quality has a major impact on what type of coagulant works best. The comparison of

Table 1

Summary of comparison of tannin coagulants to other coagulants in water and wastewater treatment.

| Water type | Tannin coagulant | Required dosage and removal efficiencies | Reference |
|--|---|---|------------------------------|
| Municipal wastewaters | | | |
| Raw municipal wastewater | Commercial TC (Acquapol C1 18, Acquachimica) | Dosage: – Total coliforms: AS ≈ TC > FAS ≈ FC > PAC <i>E. coli</i> : AS ≈ TC > FAS ≈ FC > PAC Adenovirus: AS > TC > FAS ≈ FC > PAC (pH of wastewater) | (Fabres et al., 2017) |
| Raw municipal wastewater | Commercial TC (Tanfloc, Tanac) | Dosage: TC ≈ PAC Turb.: TC > PAC BOD ₅ : TC ≈ PAC COD: TC ≈ PAC TSS: TC > PAC Tot-P: TC ≈ PAC (pH 7.2–7.9) | Hameed et al. (2016) |
| Treated municipal wastewater | Commercial TC (Tanfloc SG, Tanac) | Dosage: TC < AS Turb.: AS > TC Color: AS > TC TOC: AS > TC Culturable bacteria: AS ≈ TC ARGs: AS > TC (pH 6.6 (AS), pH 7.5 (TC)) | (Grehs et al., 2019) |
| Secondary treated municipal wastewater | Commercial TC | Dosage: Starch < Chit < TC < PAC Turb.: Chit > TC > PAC ≈ Starch BOD ₇ : Starch > TC > PAC > Chit COD: Starch ≈ TC ≈ PAC > Chit SS: TC > Starch ≈ PAC > Chit PO ₄ -P: TC ≈ PAC > Starch > Chit Tot-P: TC ≈ PAC > Starch > Chit Tot-N: TC ≈ PAC ≈ Chit > Starch (pH 6.4–6.7) | (Cainglet et al., 2020) |
| Treated municipal wastewater | Commercial TC (Acquapol 893/11, Acquachimica) | Dosage: – Total coliforms: FC > TC > PAC > FAS > AS <i>E. coli</i> : FC ≈ TC > PAC > FAS > AS Adenovirus: FC > TC > PAC > FAS > AS (pH of wastewater) | (Fabres et al., 2017) |
| Industrial wastewaters | | | |
| Blast furnace gas wash water | Commercial TC (Grove) | Dosage: PAM < TC < FS Turb.: PAM ≈ TC > FS (pH 8.0–8.1) | (Kiventerä et al., 2016) |
| Humic peat extraction runoff | Commercial TC (Grove) | Dosage: Chit ≈ PD < FS < TC DOC: FS > PD > TC ≈ Chit Tot-P: FS > PD > Chit ≈ TC Tot-N: FS > Chit > PD > TC SS: Chit ≈ TC > FS > PD (pH 6.5) | (Heiderscheidt et al., 2016) |
| Synthetic textile solution (DB85, NaCl, NaHCO ₃) | Commercial TC (Tanfloc SG, Tanac) | Dosage: FS < TC Color: FS ≈ TC (pH 4–8) | (Lopes et al., 2019) |
| Synthetic textile solution (DB85, NaCl, NaHCO ₃ , auxiliary dyeing chemicals) | Commercial TC (Tanfloc SG, Tanac) | Dosage: FS < TC Color: FS ≈ TC (pH 4 and 5) Dosage: TC < FS Color: TC > FS (pH ≥ 6) | (Lopes et al., 2019) |
| Synthetic textile solution (Reactive Blue 19, NaCl, auxiliary dyeing chemicals) | Commercial TC (Tanfloc SG, Tanac) | Dosage: RF < TC Color: RF > TC (pH 9) | (Machado et al., 2022) |
| Textile wastewater | Commercial TC (Polysep3000, AQUAREX-ARCIE) | Color: FC > TC > AS COD: AS > FC > TC (pH 8 (FC), pH 7 (AS), pH ≤ 10 (TC)) | (Aboulhassan et al., 2005) |
| Swine slaughterhouse wastewater | Commercial TC (Tanfloc SG, Tanac) | Dosage: TC ≈ PAC Turb.: TC > PAC Color: TC ≈ PAC (pH 6.6) | (Bongiovani et al., 2018) |
| Cassava processing wastewater | Commercial TCs (Acquapol WW, Acquapol SST, Acquachimica; Tanfloc SL, Tanfloc SG, Tanac) | Dosage: TCs < AS Turb.: TCs > AS Color: TCs > AS (pH 7.1) | (dos Santos et al., 2018) |
| Paint manufacturing wastewater | TC | Dosage: TC ≈ FC < AS COD: TC > FC > AS Color: TC > FC ≈ AS (optimal pH for coagulants) | (Aboulhassan et al., 2016) |
| Dairy wastewater | Commercial TC (Tanac) | Dosage: TC ≈ PAC Color: TC ≈ PAC Turb.: TC ≈ PAC | (Dela Justina et al., 2018) |

(continued on next page)

Table 1 (continued)

| Water type | Tannin coagulant | Required dosage and removal efficiencies | Reference |
|---|--|---|-------------------------------|
| Plastic recycling wastewater | Commercial TC (Tanfloc, Tanac) | COD: PAC ≈ TC TSS: TC ≈ PAC (pH 6.0–7.0) Dosage: MO < TC Turb.: MO > TC Color: MO > TC COD: MO > TC (pH 7.3) | (Ribeiro et al., 2023) |
| Tannery wastewater | TC | Dosage: TC ≈ AS Sulfide: TC > AS Turb.: AS > TC Color: AS > TC COD: AS > TC Tot.N: AS > TC | (Uez et al., 2023) |
| Other waters | | | |
| Kaolin suspension | Commercial TC (Tanac) | Dosage: PD < TC < AS Turb.: AS > PD > TC (pH 7) | (Graham et al., 2008) |
| Kaolin/river water | TCs (Spruce, Quebracho) | Dosage: TCs < FS Turb.: TC (Quebracho) ≈ FS > TC (Spruce) UV ₂₅₄ : FS > TCs (pH 7.5) | (Bello and Leiviskä 2022) |
| River water enriched with <i>Oocystis</i> algae | Commercial TCs (Acquapol C1, Acquachimica; Tanfloc, Tanac; Silvafloc, Silvateam) | Dosage: – Algae removal: TCs > cationic starch > AS (dosage of 10 mg/L) (pH 7.8) | (Barrado-Moreno et al., 2016) |

TC – tannin coagulant; Chit – chitosan; PD – PolyDADMAC; FS – ferric sulfate; PAM – polyacrylamide; AS – aluminum sulfate, PAC – polyaluminum chloride; FAS – ferrous aluminum sulfate; FC – ferric chloride; PA – polyamine; Turb. – Turbidity; DB85 – Direct Blue 85 dye; RF – Rifloc 6548; MO – *Moringa oleifera*.

purification efficiency is not so straightforward when considering same time several different water quality parameters, and since the treatments are being made with or without pH adjustments depending on the situation. Nevertheless, many studies have shown that tannin coagulants work just as well as other coagulants and sometimes even better. Fig. 1 shows the specific parameters associated with various water types, in which tannin coagulants demonstrate remarkable removal efficacy. It is worth to note that several commercial tannin coagulants are available, such as Tanfloc and Acquapol.

2.2.1. Turbidity, organic matter and nutrients removal

Few studies have compared tannin coagulants to other coagulants in the treatment of municipal wastewaters. Grehs et al. (2019) showed that both AS and tannin coagulant removed well turbidity, color, total organic carbon (TOC), and culturable bacteria from municipal wastewater effluent. The main difference was that AS decreased the analyzed antibiotic resistance genes (ARG) content to a lower level than the TC, and that the TC-treated effluent showed bacterial reactivation after storage. Hameed et al. (2016) showed that the tannin coagulant achieved higher removal of turbidity than polyaluminum chloride (PAC, pH 7.9) in a raw municipal wastewater (dosage 35 mg/L for both coagulants). On the other hand, chemical oxygen demand (COD), biological oxygen demand (BOD), and total phosphorus (Tot-P) removals were not significantly different with studied coagulants. In a study by Fabres et al. (2017), several commercial tannin coagulants were tested for total coliform bacteria, *Escherichia coli*, and adenovirus removal from raw and treated municipal wastewaters. In raw wastewater, AS achieved the best removal rates, followed by the Acquapol C1 18 tannin coagulant. In

treated wastewater, ferric chloride (FC) and Acquapol 893/11 tannin coagulant resulted in best performance. The study also showed that among tested tannin coagulants, significant differences in purification results were observed. This underlines the important fact that different tannin raw materials and modification conditions will affect the properties of the tannin coagulant, and the optimal tannin coagulant needs to be tested in the application. Cainglet et al. (2020) tested PAC, several polyDADMACs, and polyamines with different molecular weights (MW), chitosan, and starch- and tannin-based coagulants in the treatment of municipal wastewater collected from the secondary sedimentation stage. In general, tannin coagulant performed well, although some higher dosages were needed (except PAC, which needed an even higher dosage). High-MW polyamine achieved the best removal of suspended solids (SS), phosphate-phosphorus (PO₄-P), and BOD₇.

In surface water treatment, tannin coagulants have been investigated for the removal of algae, turbidity, and natural organic compounds. Barrado-Moreno et al. (2016) reported that tannin coagulants removed to a higher extent *Oocystis* algae from surface water than cationic starch (Optifloc, Kemira) and AS when coagulants were applied with constant dosage (10 mg/L). Acquapol C1 tannin coagulant was selected for further studies and also proved to have a stable efficiency at a pH range 5–9 with constant dosage. The good performance of Acquapol C1 tannin coagulant was also verified in pilot tests, in which algae removal reached 90% removal in the coagulation process (at neutral pH) and was further improved after sand filtration. Bello and Leiviskä (2022) observed that tannin coagulants provided lower residual turbidities with lower dosages (25 and 50 mg/L) in kaolin/river water (pH 7.5) when compared to ferric sulfate (FS). As the pH decreased with increasing FS

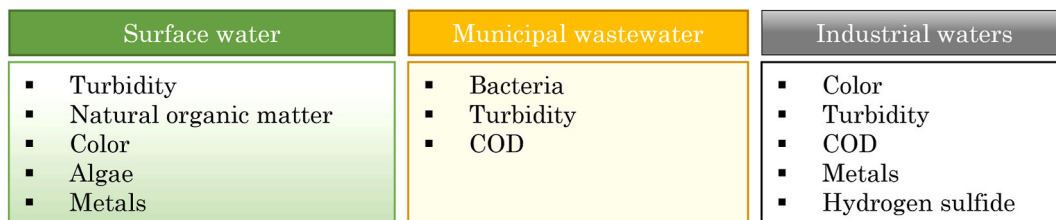


Fig. 1. Tannin coagulants applications: parameters typically well removed by TC.

dosage, very low residual turbidity was also observed with 125 mg/L FS and even lower UV_{254} values than with the tannin coagulants.

Many studies have compared tannin coagulants to other coagulants in the treatment of industrial wastewaters. In the treatment of cassava processing wastewater, several tannin coagulants (Acquapol WW and S5T, Tanfloc SL and SG) were tested at neutral pH and achieved better color and turbidity removal than AS (dos Santos et al., 2018). Among tannin coagulants, Acquapol S5T and Tanfloc SL resulted in the most efficient performance.

No significant difference was observed between tannin coagulant (*Acacia mearnsii*, Tanac) and PAC when used for dairy wastewater treatment at pH 6–7 (Dela Justina et al., 2018). The study, however, showed that the tannin coagulant had certain benefits over PAC, such as lower alkalinity consumption and lower impact on conductivity of treated water. Also, when the effect of pH was studied, tannin coagulant removed well turbidity and color in the pH range 5–10, but significantly lower efficiency was recorded at pH 4 (Dela Justina et al., 2018). PAC, on the other hand, worked well in a slightly narrower pH range (6–10).

In paint manufacturing wastewater, tannin coagulant removed the best COD and color compared to FC and AS (Aboulhassan et al., 2016). The coagulation pH did not significantly affect tannin coagulant efficiency on COD removal, while metal salts removed less COD at alkaline pH (Aboulhassan et al., 2016). In addition, in contrast to metal salts, tannin coagulant did not significantly affect the pH of the treated water, which would allow water to be led directly into the biological process.

In the case of synthetic textile effluents, tannin coagulant was more efficient than FS when the treatment was carried out at neutral or alkaline conditions (Lopes et al., 2019). However, lowering the pH of the effluent to 4 or 5, the required dosage of both tannin coagulant and FS was lower, and additionally FS provided decolorization at much lower dosages. In another study with synthetic textile effluent at pH 9, synthetic organic coagulant (Rifloc 6548) had better cost-efficiency and better color removal (81%) than tannin coagulant (42%) (Machado et al., 2022). In a study made with real textile wastewater (Aboulhassan et al., 2005), tannin coagulant achieved a high color removal (90.7%) and sufficient COD removal (50.2%), while the removal rates were higher for FC (color 97.6%, COD 57.4%). AS achieved the highest COD removal (87.2%) but the lowest color removal (71.4%).

Tannin coagulants have also been tested in combination with other coagulants. Grenda et al. (2020) showed that using tannin coagulant together with a small amount of cationic polyacrylamide (PAM) resulted in high turbidity and color removal from industrial effluent. High turbidity reduction from biologically treated industrial dyeing and laundry effluent was achieved by using both Tanfloc and cationic PAM (Costa et al., 2018). A combination of tannin coagulant (Organo-floc) and anionic PAM was successfully applied for biologically treated landfill leachate and resulted in high color removal at pH 5 (Ibrahim and Yaser 2019). Aboulhassan et al. (2006) found that the most suitable combination for the treatment of paint wastewaters would be FC, tannin coagulant and, anionic high-MW PAM when considering the sludge volume and purification results. In the treatment of turbid wastewater from plastic recycling industry, addition of magnetite nanoparticles improved the performance of tannin coagulant in terms of turbidity and color removal (Ribeiro et al., 2023). In case with *Moringa oleifera*, magnetite addition did not provide significant difference. In tannery wastewater, combining tannin coagulant with AS (in a 50:50 ratio) provided higher removal of hydrogen sulfide from wastewater (Uez et al., 2023).

2.2.2. Metal removal

Tannin coagulants have also proved to be effective in metal removal. Lugo et al. (2020) showed that copper, chromium, and mercury were most efficiently removed by *Acacia* tannin coagulant at alkaline pH from industrial wastewater (spiked with metals). This was due to higher degree of ionization of phenolic groups and stronger electrostatic attraction between metal ions and negatively charged surface of the tannin

polymer. Commercial Tanfloc MTH proved to remove above 93% of aluminium, iron and manganese from turbid river water (de Oliveira et al., 2022). In the treatment of humic peat extraction runoff water, a tannin-based coagulant was able to remove 94% of iron, whereas the application of FS led to an increase in the metal level in the water (Heiderscheidt et al., 2016). Righetto et al. (2021) examined the effectiveness of coagulation as a pretreatment technique to remove metals and improve landfill leachate quality for subsequent nutrient recovery. Using a commercial tannin coagulant (derived from the bark of the *A. mearnsii* tree), they obtained high removal efficiencies for iron and titanium (>90%) and chromium (68%) at pH 7.3. Smaller percentages (33–52%) were found for aluminum, barium, vanadium, and manganese. It is important to highlight that metal removal may also be induced by pH adjustment to alkaline conditions, as precipitation of metal ions may occur quantitatively, depending on the pH, water characteristics, and the solubility product of the metal hydroxides. Arsenic contamination in groundwater is a major problem for which coagulation-flocculation and tannin coagulants could work, but are yet to be explored. According to the authors' best knowledge, only conventional chemical coagulants have been studied (Amiri et al., 2022).

2.3. Floc characteristics and sludge quality

Properties of the flocs generated by tannin coagulants and sludge amounts have been investigated in few studies and also compared to some conventional coagulants. Floc growth, size and resistance are being affected by the wastewater or suspension quality (pH and compounds). Sludge volume and amount are also important parameters due to high costs of sludge disposal.

Graham et al. (2008) found that tannin coagulant provided a higher coagulation rate and degree of floc growth in kaolin suspension at pH 9 compared to pH 7. Coagulation rate at pH 9 by the tannin coagulant was also higher than that for the polyDADMAC at pH 7, and the degree of floc growth was higher than that of AS at pH 7. Hameed et al. (2016) found that tannin coagulant produced bigger flocs with a faster settling rate than PAC in urban wastewater treatment. After 2 min settling time, Tanfloc had removed 70% of turbidity, while PAC removed only 30%. Sludge volume indexes were at a similar level for both coagulants up to 60 mg/L dosages. In dairy wastewater treatment, tannin coagulant presented higher resistance to floc breakage than PAC during slow-mixing time and at higher velocity gradients (Dela Justina et al., 2018), which is an advantage in turbulent flows.

In textile wastewater, the tannin coagulant produced a smaller sludge volume than FC and AS, but an intermediate sludge weight between FC and AS (Aboulhassan et al., 2005). In paint manufacturing wastewater, tannin coagulant produced less volume of decanted sludge than FC and AS (Aboulhassan et al., 2016). Similar results were found in tannery wastewater treatment, in which FS generated higher sludge volume without sufficient settling characteristics (sludge volumetric index above 100 mL/g), compared to the tannin coagulant (Aboulhassan et al., 2021). Sludge volume of municipal wastewater of the secondary sedimentation stage was decreased when tannin coagulant was applied (Cainglet et al., 2020). However, starch, chitosan, high-MW polyamine, and high-MW polyDADMAC achieved an even higher decrease in sludge volume. On the other hand, polyamine and polyDADMAC with lower MW as well as PAC did not have a decreasing effect on the volume of sludge produced.

The use of plant-based coagulants also allows for a safer disposal of the sludge, compared to conventional coagulants, and may be a route for nutrient recovery through the application of the generated sludge as fertilizer in agriculture, as proposed by Alnawajha et al. (2022) for aquaculture wastewater treatment.

Table 2

Maximum adsorption capacities (Q) reported in literature for tannin-derived adsorbents, and different organic and inorganic contaminants.

| Adsorbate | Adsorbent | Q (mg/g) | Reference |
|---------------------------------|--|---------------------|-------------------------------|
| Metal removal | | | |
| Cd(II) | Bayberry tannin polymer immobilized on cellulose | 73.6 (298 K, pH 5) | (Zhou et al., 2019) |
| Cr(VI) | Black wattle tannin-gel | 488 (298 K, pH 1) | (Rodrigues et al., 2015) |
| Cr(VI) | Black wattle tannin-immobilized nanocellulose | 105 (pH 2) | (Xu et al., 2017) |
| Cr(VI) | Gelatin-chestnut biopolymer | 80.6 (298 K, pH 4) | (Hassoune et al., 2018) |
| Cr(VI) | MnO ₂ -PEI-TA composite | 790 (298 K, pH 2) | (Deng et al., 2021) |
| Cr(VI) | Biomaterial from chestnut tannin with proteins hydrolysate from wet blue chrome shavings (CT-PH) | 40.16 (298 K, pH 3) | (Nechchadi et al., 2022) |
| Cr(VI) | Persimmon tannin functionalized waste paper | 178.7 (298 K, pH 2) | (Liu et al., 2022) |
| Cu(II) | Tannin-PEI adsorbent | 80 (298 K, pH 5) | (Jiang et al., 2020) |
| Cu(II) | Black wattle tannin-immobilized nanocellulose | 52 (298 K, pH 6) | (Xu et al., 2017) |
| Cu(II) | Bayberry tannin polymer immobilized on cellulose | 53.19 (298 K, pH 5) | (Zhou et al., 2019) |
| Cu(II) | MnO ₂ -PEI-TA composite | 125 (298 K, pH 5.5) | (Deng et al., 2021) |
| Hg(II) | Tannic acid film covered magnetic microspheres | 279 (303 K, pH 6.0) | (Luo et al., 2017) |
| Pb(II) | Silverwattle tannin resins | 189 (pH 6) | (Okoli et al., 2018) |
| Pb(II) | Black wattle tannin-immobilized nanocellulose | 53 (pH 6) | (Xu et al., 2017) |
| Pb(II) | Tannic acid film covered magnetic microspheres | 1115 (303 K, pH 6) | (Luo et al., 2017) |
| Pb(II) | Tannin-based magnetic POP | 252 (pH 5) | (Huang et al., 2019) |
| Pb(II) | Self-assembled metal-phenolic networks | 356.1 (pH 5, 298 K) | (Qiu et al., 2022) |
| Zn(II) | Pinus tannin gel | 65 (293 K, pH 7) | (Sánchez-Martín et al., 2011) |
| Radionuclides removal | | | |
| U(VI) | Polytannin (<i>A. nilotica</i> fruit) glutaraldehyde resin | 104 (298 K, pH 3) | (Alhumaimess et al., 2019) |
| U(VI) | Persimmon tannin functionalized waste paper | 242.3 (298 K, pH 6) | (Liu et al., 2022) |
| U(VI) | Tannin grafted bovine serum albumin nanospheres | 488 (pH 5) | (Yu et al., 2018) |
| Toxic metalloids | | | |
| As(III) | Fe ₃ O ₄ @TA@UiO-66 microsphere | 97.8 (RT) | (Qi et al., 2019) |
| As(V) | Iron-loaded pine bark tannin resin | 0.7 (293 K, pH 3) | (Bacelo et al., 2020) |
| Sb(III) | Pine bark tannin resin | 32.9 (298 K, pH 6) | (Bacelo et al., 2018) |
| Sb(V) | Pine bark tannin resin | 47 (298 K, pH 2) | (Bacelo et al., 2022) |
| Sb(III) | Fe ₃ O ₄ @TA@UiO-66 microsphere | 49.5 (RT) | (Qi et al., 2019) |
| Color removal | | | |
| MB | Pinus tannin gel | 499 (293 K, pH 7) | (Sánchez-Martín et al., 2011) |
| MB | Tannin-immobilized cellulose microspheres | 57.5 (303 K, pH 8) | (Pei et al., 2017b) |
| MB | Tannin-based magnetic POP | 1696 (natural pH) | (Huang et al., 2019) |
| MB | Iron-polyphenol nanomaterial | 187 (pH 7) | (Aktar and Ray 2022) |
| DY86 | Oak gall tannin-immobilized HMS | 436 (293 K, pH 2) | (Binaeian et al., 2016) |
| MO | APTES-functionalized tannin-rich grape biomass | 314.6 (298 K, pH 6) | (Cavalcante et al., 2022) |
| AR1 | Tannin-APTES adsorbent | 217 (298 K, pH 2) | (Leite et al., 2017) |
| Pharmaceutical compounds | | | |
| CIP | Fe-modified bayberry tannin foam | 112 (298 K) | (Hao et al., 2021) |
| DIC | Tannin from Indian almond leaf | 71.9 (298 K) | (Sunsandee et al., 2020) |

AR – Acid Red; CIP – ciprofloxacin; DIC – Dicloxacillin; DY – Direct Yellow; HMS – hexagonal mesoporous silicate; POP – porous organic polymers; RT – room temperature; TA – Tannin acid.

3. Tannin-derived adsorbents for water treatment

3.1. Tannin resins

Resins (or gels) result from the insolubilization of tannins through alkali- or acid-catalyzed polymerization with formaldehyde. This reaction primarily takes place at the nucleophilic centers on the A-ring (more reactive than B-ring sites), creating methylene bridges and forming a cross-linked three-dimensional structure (Arbenz and Averous 2015; Xiaojian and Guanben 2019). Formaldehyde effectively cross-links condensed tannins, enabling the development of sorbents from various sources such as pine bark, quebracho, cypress, and Weibull black tannin (Sánchez-Martín et al., 2011; Bacelo et al., 2020). Concerns regarding formaldehyde toxicity have motivated the use of alternative cross-linking agents, such as benzaldehyde (Okoli et al., 2018) and glutaraldehyde (Alhumaimess et al., 2019), though with lower reactivity. Autocondensation reactions are characteristic of polyflavonoid tannins (Xiaojian and Guanben 2019) and may be alternative routes for insolubilizing tannin molecules without aldehydes. In some instances, a catalyst is required as exemplified for persimmon tannin, converted into successful sorbents through boiling in concentrated sulfuric acid (Inoue et al., 2015). Studies conducted on wattle tannin-formaldehyde gelation show that tannin gels generated under acid conditions tend to develop higher pore volumes (Amaral-Labat et al., 2013; Braghiroli et al., 2019),

whereas materials with smaller no appreciable pores are generated in alkaline conditions. The authors have also pointed out that shrinkage and porosity loss can occur in the drying process (Amaral-Labat et al., 2013). Indeed, most tannin resins evaluated as sorbents present minor surface areas (Sánchez-Martín et al., 2011; Okoli et al., 2018; Bacelo et al., 2020), despite showing good adsorptive properties, explained by the abundant phenolic hydroxyl groups prone to form stable chelates with metal ions (Koopmann et al., 2020). The ionization of these groups and stabilization by resonance generate a negative surface charge in practically the entire pH range, as indicated by isoelectric points measured at approximately pH 2 (Rodrigues et al., 2015; Sun et al., 2021; Bacelo et al., 2022). This feature enables electrostatic interactions with cationic adsorbates in a wide pH range, and explains the efficient uptake of various metals from water, such as Cd(II), Cu(II), Pb(II), Zn(II), and cationic organic species, such as methylene blue dye (MB). This is depicted in Table 2, which presents data collection on the maximum adsorption capacities reported for tannin sorbents (experimental or calculated values from valid equilibrium models). In addition to the electrostatic attraction, hydrogen bonds and van der Waals interactions explain significant uptake ability organic micropollutants such as dicloxacillin antibiotic (Sunsandee et al., 2020).

Removing radioactive elements from water, such as hexavalent uranium, is another potential use of tannins. Alhumaimess et al. (2019) synthesized a polytannin glutaraldehyde resin from *Acacia nilotica* fruit

tannin, starting by reacting with formaldehyde followed by glutaraldehyde cross-linking. The material presented a rapid removal of U(VI) from water (60–90 min), efficient in the pH range of 3–6, and optimum adsorption at pH 6.

Tannin resins are also good sequestrants of metal(loid)s species that appear in water under anionic or neutral complexes, such as hexavalent chromium and antimony. In acidic and neutral conditions, Cr(VI) is present in water under the anionic species HCrO_4^- and $\text{Cr}_2\text{O}_7^{2-}$ and therefore its uptake through electrostatic attraction is not possible. The outstanding adsorptive ability, exemplified for a black wattle tannin gel is explained by Cr(VI) adsorption by phenolic groups via chromate esterification, reduction of part of Cr(VI) to Cr(III) with the oxidation of phenolic hydroxyls in tannin; and Cr(III) uptake by electrostatic attraction (Rodrigues et al., 2015). A tannin resin polymerized from maritime pine bark extract showed great adsorption affinity for antimony, in particular for the most toxic species of Sb(III), which can be quantitatively removed from water in a wide pH range by complexation with adjacent hydroxyl groups on tannin sorbents (Bacelo et al., 2018).

In a different synthesis approach, a biobased phenolic resin was prepared through the polymerization of a blend of condensed tannin (black wattle commercial sample) and crude industrial Kraft black liquor (Moreira et al., 2022). The procedure involved several steps, starting with hydroxymethylation of the raw Kraft black liquor with formaldehyde, followed by mixing with tannin and sodium hydroxide mixture and ending with a thermal treatment at 170 °C. The biobased resin was able to provide 100% removal of metals from aqueous solution, being also quite effective in Diuron and methylene blue uptake but ineffective for methyl orange and atrazine. The authors concluded that more lipophilic compounds (highest distribution coefficient value) are more extensively removed.

3.2. Amine-functionalized tannin adsorbents

Amine functionalization based on hydrogen bonding between materials containing hydroxyl and amino groups has been highly investigated to generate tailored tannin resins. Introducing N-containing functions and replacing some hydroxyl groups create positively charged centers in the adsorbent surface. The pH range where the adsorbent assumes a positively charged surface is typically extended, and the adsorption performance is enhanced. The isoelectric points of tannin resins have been identified at a pH around 2, whereas a pH of 7.7 was obtained for a triethylamine-modified tannin gel (Shan et al., 2015). Different routes can be used to anchor N-ligands to tannins. Akter et al. (2016) prepared an amine-modified adsorbent by reacting a formaldehyde cross-linked tannin resin with ammonia. They confirmed a slightly higher performance of the resulting sorbent towards a cationic dye. Jiang et al. (2020) synthesized a composite using only tannin and polyethylenimine (PEI), a polymer with many repeating units containing amino groups. A first step in which hydrogen bonds formed between hydroxyl groups on tannin and amino groups on PEI was followed by continuous stirring and polymerization without the need of cross-linking agents. The synthesized adsorbent was effective in Cu(II) removal from water. The more interesting advantage of amino modification, however, is the removal of anionic adsorbates, which is usually more challenging. Binaeian et al. (2016) synthesized aminated hexagonal mesoporous silicate nanoparticles and further immobilized oak gall tannins using glutaraldehyde. The synthesized material showed a good adsorption capacity for the anionic dye Direct Yellow 86. Dye removals by aminated and non-aminated hexagonal mesoporous silicate nanoparticles, and oak gall tannin-immobilized adsorbent were compared. The improvement in dye uptake was attributed to the tannin incorporation, but amination has conferred the greatest improvement in the decolorization efficiency. Composites prepared by reacting tannins with APTES (3-aminopropyltriethoxysilane) at 75 °C using ammonia presented great adsorption capacities for the anionic dye Acid Red 1, especially at pH 2, under which the amino groups are protonated and able to interact

electrostatically with the anionic dye (Leite et al., 2017). Cavalcante et al. (2022) grafted a tannin-rich grape residue with APTES in a single step 80 °C procedure. Although the smooth shift in the isoelectric point from 1.8 to 2.8, the functionalization generated enhanced chemical surface activity and a sorbent with remarkable adsorption capacity for methyl orange dye (Table 2). Although acidic conditions favored dye uptake due to an electrostatic attraction mechanism, pH 6 was considered a more realistic pH for adsorption assays.

3.3. Iron-tannin composites

Iron-based adsorptive media are usually suitable for pollutant removal from water, in particular for arsenic, radium, uranium, and antimony. Tannin resins or foams are also possible carriers of iron, owing to the high affinity of B-ring hydroxyl groups of the condensed tannins to transition metals and to the stability of complexes formed with iron(III) (Koopmann et al., 2020). Bacelo et al. (2020) prepared an iron-loaded tannin resin, starting with formaldehyde cross-linking of pine bark tannins, followed by partial oxidation with hot nitric acid and Fe(III) loading. The intermediate oxidation step was found important for the subsequent iron uptake, as some catechol hydroxyl groups oxidized to carbonyl groups, which have a higher affinity to iron ions. Hao et al. (2021) synthesized a foam from bayberry tannins using hexamethylenetetramine as a cross-linker. The resulting material preserved phenolic hydroxyls and was a porous supporting matrix for Fe(III) via coordination. Negative zeta potentials in almost the entire pH range were reported despite the iron modification, restraining the chances for electrostatic attraction with anionic adsorbates. Iron-tannin composites showed certain adsorption ability for arsenic(V), compared to unmodified tannin resins which presented negligible adsorption (Bacelo et al., 2020). Hao et al. (2021) reported successful removal of ciprofloxacin (an antibiotic) from water demonstrating that the metal was the main responsible for the observed efficiency. Qiu et al. (2022) prepared polyphenol-based adsorbents using tannic acid and ferric ions through simple cross-linking self-assembly reactions and indicated an excellent adsorption capacity for lead(II), assigned to the strong coordination between the metal and phenolic hydroxyl and ester groups, and specific adsorption on the newly formed hydrous ferric oxides.

3.4. Tannin composites using natural substrates

The use of natural polymers as substrates for tannin immobilization strengthens their functional performance, as they can be dispersed in a more suitable morphology for continuous processes and may provide high adsorption ability and efficient adsorption rate (Guan et al., 2023). The natural abundance and easy chemical modification of cellulose have motivated research on its use as a carrier to immobilize tannins. One of the main strategies to form covalent bonds for conjugating tannins and cellulose is using epichlorohydrin (ECH) as a crosslinker. Pei et al. synthesized tannin-immobilized cellulose microspheres and hydrogels via homogeneous reaction, using ECH and condensed tannins from *Areca catechu* fruits (Pei et al. 2017a,b; Pei et al. 2019). Zhou et al. (2019) proposed a tannin-phenolic polymer produced from bayberry tannins through paraformaldehyde cross-linking and cellulose immobilization by ECH. The authors argued that tannins insolubilization before immobilization on cellulose increases the effective phenolic hydroxyl content in the cellulose skeleton and enhances the adsorptive properties of the adsorbent. These cellulose-tannin composites showed a great potential to clean up waters from Cd(II), Cu(II), Pb(II), and cationic dye (Table 2), mainly due to the negatively charged surface and electrostatic-based adsorptive mechanism. The other approach to conjugate cellulose substrates with tannin derivatives is reported by Xu et al. (2017). A black wattle tannin-nanocellulose composite was prepared starting by oxidizing nanocrystalline cellulose using sodium periodate to get dialdehyde nanocellulose, which served as the matrix and cross-linker. Black wattle tannin did not leak out during the

adsorption process, indicating tight immobilization onto nanocellulose by covalent bonding. In other work, dialdehyde waste paper was used as a cross-linking agent to immobilize persimmon tannin into a nanocomposite (Liu et al., 2022). The waste paper mainly comprises cellulose and hemicellulose and is easily oxidized, generating a mass of aldehyde that can be used to dismiss cross-linking agent usage. The persimmon tannin functionalized waste paper sorbent presented an isoelectric point of 4.18 and great potential to remediate U(VI) and Cr(VI) contaminated water, reaching adsorption capacities of 242 and 179 mg/g at pH 6 and 2 (Table 2), respectively. U(VI) uptake is mainly dependent on chelation, whereas the Cr(VI) adsorption might stem from a combination of electrostatic attraction and redox reaction. In another work, a cellulose nanofiber-based adsorbent was prepared by introducing persimmon tannin/MXenes-NH₂ into dialdehyde cellulose nano-fibres. Characterization indicated plenty of functional groups (Ar-OH, -NH₂, Ti-OH), providing rich active sites for radionuclides uptake from water (Liu et al., 2023).

Immobilization of tannins on collagen and gelatin through covalent and non-covalent binding (hydrogen bonds and hydrophobic interactions) has also been reported in the literature (Guan et al., 2023). Meng et al. (2019) prepared a composite assembling gelatin, PVA (poly vinyl alcohol), and bayberry tannin by electrostatic spinning and crosslinking by glutaraldehyde. The results revealed that the tannin had been stably solidified on the composite, which showed great potential to adsorb uranium from simulated seawater. Hassoune et al. (2018) prepared biopolymers by precipitating gelatin extracted from untanned hide wastes with chestnut and quebracho tannins. Although the derived biopolymers seem to be less effective for Cr(VI) than tannin resins, the adsorption mechanism is referred to be the same. Moreover, the material cannot be used at strongly acidic and alkaline media, in which the composite is unstable.

Bayberry tannin can also be immobilized into other proteins, such as bovine serum albumin nanospheres (Yu et al., 2018). The developed sorbent efficiently removed uranyl ions from radioactive wastewater due to a chelating mechanism between UO₂²⁺ and the adjacent phenolic hydroxyls and chelating sites such as =CO and -NH₂ on the serum albumin.

3.5. Tannin-based nanoparticles and magnetic sorbents

Nanoadsorbents synthesized from various materials are a promising approach for water purification. Their potential stems from the high adsorption capacities and rapid sorption kinetics, attributed to the large surface area, and can be enhanced through various engineered chemical modifications. Recently, several tannin-based nanostructured sorbents were investigated for water purification including oak gall tannin-immobilized hexagonal mesoporous silicate nanoparticles used for anionic dye removal (Binaeian et al., 2016), iron-polyphenol nanomaterial investigated, able to remove fluoride and cationic dye from water and whose synthesis process can be replicable in large quantities (Aktar and Ray 2022), and a black wattle tannin-nanocellulose composite successfully tested for metal adsorption (Xu et al., 2017). Persimmon tannin nanocomposites (Liu et al., 2022) and gelatin/PVA composite nanofiber band loaded with bayberry tannin (Meng et al., 2019) were proposed for uranium uptake. Despite the observed good performance of nanosorbents at the laboratory scale, their use on full-scale may be challenging due to their handling and safety concerns and difficult separation (Mudhoo and Sillanpää 2021). Magnetic nanosorbents have been the target of intense research, as they allow an easy solid-liquid separation provided by an external magnetic field. Tannin immobilization in magnetic particles, composed of an iron oxide core and a silica shell, has been proposed by several authors. Luo et al. (2017) prepared tannin acid film covered magnetic nanoparticles (Fe₃O₄@TA-Fe³⁺). Great adsorption abilities were obtained for Pb(II) and Hg(II) (see Table 2). Huang et al. (2019) developed tannin-based magnetic porous organic polymers (POPs). As it can be seen from

Table 2, the adsorbent presented remarkable and fast uptake of Pb(II) and MB pollutants from water due to the high surface area, abundant phenolic groups, and negatively charged surface at pH above 3. Considering that UiO derivatives are a promising methodology for As (III) and Sb(III) sequestering, a magnetic core-shell nanocomposite was designed, where polyphenol tannic acid acted as a modifier and bridge, connecting UiO-66 MOF (metal-organic framework) particles to the magnetic Fe₃O₄@TA (Qi et al., 2019). The removal mechanism was mainly attributed to complexation involving Zr-O-As and Zr-O-Sb bonds, but the abundant hydroxyl groups of tannic acid facilitated the uptake of the adsorbates.

3.6. Application potential

Different tannin-derived materials have been developed to remove of inorganic and organic contaminants from water, with potential for various applications, according to available literature (Fig. 2). It is, however, important to discuss several points related to the practical application. One of them is the possible interference of coexisting species in the solution. Most studies have been conducted using synthetic solutions (containing the adsorbate dissolved in water), but some others evaluate the adsorption performance under complex and real water matrices. No drastic interferences have been reported for lead uptake considering metal removal in water treatment or industrial effluent remediation. Luo et al. (2017) tested magnetic tannin composites for Pb (II) and Hg(II) removal in tap and lake water. Although a certain decrease in the adsorption capacity was obtained for Pb(II) (roughly a 30% decrease), compared to a simple aqueous solution, the adsorbent still presented an outstanding ability to sequester the metal (more than 750 mg/g). A negligible effect of the aqueous matrix was observed for mercury uptake. Qiu et al. (2022) indicated that most cations (Zn(II), Cd (II), Ca(II), Mn(II), and Mg(II)) exert little effect on Pb(II) adsorption by a polyphenol-based adsorbent, oppositely to Ni(II) and Cu(II) which can reduce the adsorption capacity of the material, but do not compromise sorbent efficiency. Aktar and Ray (2022) validated the fluoride uptake performance of an iron-polyphenol nanomaterial on groundwater samples collected in India. The adsorbent was able to reduce fluoride levels to recommended permissible limit (1.5 mg/L), by adjusting dosages between 2 and 3 g/L.

Bacelo et al. (2022) observed that the breakthrough in an adsorptive column containing pine bark tannin resin was reached faster and the sorbent usage efficiency decreased roughly to two-thirds when the column was fed with a simulated mine effluent, compared to a single metal solution. High sulfate levels characterize most mining-impacted waters, but the adsorbent's performance towards Sb(III) remained unaffected in the presence of this background ion. In contrast, high levels of calcium and magnesium ions moderately affect the antimonite uptake.

In organic micropollutants, dye removal from textile dyehouse effluents is another potential application (Table 2). Conventional treatment processes are not completely effective for textile effluent remediation, and a final refining treatment step of adsorption can be considered to achieve total decolorization. However, literature has been mostly focused on basic (cationic) dyes removal (e.g., MB), and few studies have been conducted using reactive dyes (widely applied to dye cotton and of particular challenging removal). In addition, complex aqueous matrices, typically characterizing textile effluents should be tested. Some potential of tannin sorbents is also expected for wastewater generated in pharmaceuticals production but with high specificity considering chemical properties of the adsorbates. Sunsandee et al. (2020) showed the performance of immobilized almond leaf tannins on dicloxacillin uptake, using a real effluent containing solvents, additives, and reactants.

Packed beds are the most used adsorbents in full-scale adsorption. Small particles are not amenable to adsorption columns due to the pressure drop, and a few studies address coarser particles or fixed bed column studies. Bacelo et al. (2022) employed a tannin resin in a packed

















| Ground/Surface water | Metal finishing effluents | Textile wastewater | Mining wastewater |
|--|--|---|--|
| Arsenic   | Heavy metals   | Basic dyes (cationic)  | Heavy metals  |
| Antimony   | Radioactive wastewater | Acid, direct & reactive Dyes (anionic)  | Arsenic   |
| Heavy metals  | Uranium(VI)  | | Antimony   |
| Pharmaceuticals  | | | |

Fig. 2. Potential applications of tannin-derived adsorbents: TRC – Tannin resins and composites; FeTR – Iron-loaded materials; AFT – Amine-functionalized materials; TMOF – Tannin-MOF composites.

bed for Sb(III) uptake and the adsorptive capacity obtained was practically the same as the one found in batch mode. The authors indicate an adsorbent usage rate as low as 0.11 kg/m³ to treat efficiently (90% removal) 1 mg-Sb/L aqueous solution, that could represent an Sb-contaminated groundwater. Qiu et al. (2022) reported that the metal-phenolic network they produced can produce 9500 and 7860 bed volumes of clean water, with Pb(II) levels below 1 mg/L, when fed with synthetic polluted and simulated electroplating wastewater. As an alternative to column processes and to the need for coarser particles, magnetic tannin particles can be applied in stirred adsorbents, offering feasible solid-liquid separation.

The regeneration of the adsorbents is also a critical factor for the cost-effectiveness of the process. Desorption, regeneration and reuse of tannin-derived adsorbents on uptake of cationic dye and metals (Pb and Cu ions) have been reported with practically no loss of adsorption efficiency (<10%) for 4–5 adsorption/desorption cycles. The eluents used are acid solutions (Xu et al., 2017; Huang et al., 2019; Jiang et al., 2020), and the desorption provided is probably due to the reversal of the electrostatic attraction mechanism. In contrast, tannin sorbents saturated with antimony or chromium(VI) presented a challenging regeneration, using alkaline and acid solutions, respectively (Xu et al., 2017; Bacelo et al. 2018, 2022). Despite the chromium can be desorbed with

nitric acid solution, a poor adsorption performance after regeneration was found, attributed to an adsorption mechanism based on redox reaction. Fig. 3 summarizes the author’s perspective on the strengths, weaknesses, opportunities, and threats related to this matter.

4. Conclusions

The market needs for water treatment chemicals produced from renewable resources is evident. Tannin’s role in the future production of natural-based coagulants and adsorbents for water purification is increasingly recognized. Tannin coagulants have demonstrated remarkable efficacy across various applications, often surpassing the performance of conventional coagulants. A key advantage of tannin coagulants is their minimal impact on the pH of treated water. This characteristic proves particularly beneficial when it is necessary to maintain a specific pH level for subsequent processes. Also, many studies have concluded that tannin coagulants can work at a wide pH range (although the required dosage can vary), and sludge volume is smaller than with metal salts. However, more research is needed on different types of wastewater at a larger scale and to compare tannin coagulants with other bio-based coagulants. It is worth noting that the performance of tannin coagulants also varies widely among tannin coagulants since

| Strengths | Weaknesses |
|--|---|
| Valorization and efficient use of locally available vegetable materials Response to market needs Possible integration in a biorefinery concept Simple routes required for extraction and coagulants and adsorbent synthesis, and for tailoring sorbents Different tannin adsorbents forms Broad range of application of tannin coagulants and adsorbents Low pH dependence of coagulants (lower operating costs and more consistent performance) Foster water remediation and reuse Reduce external dependence from water treatment chemicals (important mainly for low-income countries) Regeneration of exhausted sorbents or direct reuse in catalysis or construction materials Valorization of the generated sludge (e.g., agriculture) | Seasonal changes in raw materials can affect impurities in extract The most established routes for coagulants and adsorbents synthesis require formaldehyde use, which is toxic Chemical instability of some chemical modified tannin sorbents and coagulants (increase in organic matter and N in water – possible secondary pollution; limited potential for drinking water production) Inefficient performance of adsorbents for specific highly toxic adsorbates such as arsenic Removal of certain pollutants by tannin sorbents requires unfeasible pH adjustment |
| | Unknowns |
| | Lack of systematic studies confirming performance under full scale (coagulation/flocculation and adsorption) and employing actual water or effluents Economic assessment (possible critical for certain chemical modified adsorbents) Green label depends on life-cycle assessment |

Fig. 3. Strengths, weaknesses, opportunities and threats of tannin coagulants/flocculants and adsorbents usage for water purification: authors perspective.

tannin raw material, modification conditions, and impurities affect the characteristics of tannin coagulants. In addition, tannin coagulant synthesis should continue to be investigated to go further on greener procedures and avoid organic matter or nitrogen leaching from tannin coagulants, which limits the application for drinking water treatment purposes. The tannin coagulant costs have been highlighted as still uncompetitive.

Various tannin-derived adsorbents have been synthesized for pollutant uptake from water. Strengths of tannin adsorbents lie in the use of locally available natural materials as precursors, synthesis processes with low chemicals and energy requirements, the possibility to prepare adsorbents in different particle sizes or to magnetize them, excellent and fast uptake of a broad range of metals, radionuclides, and organic compounds. Weaknesses are identified in the limited ability to uptake certain adsorbates, such as arsenic and anionic dyes, requiring amine-functionalization or MOF composites, involving additional processing and higher synthesis costs. More research is needed to validate the identified application fields.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data availability

No data was used for the research described in the article.

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